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(54) **Methods for the preparation of liquid silicone rubber base and liquid silicone rubber composition**

(57) A liquid silicone rubber base is prepared by mixing an organopolysiloxane containing at least two alkenyl groups, reinforcing silica having a BET specific surface area of at least 50 m<sup>2</sup>/g, and optionally, a mixing assistant. The mixing step includes a first stage of mixing

under a first shear stress of at least 1x10<sup>6</sup> N/m<sup>2</sup> for 1-5 minutes and a second stage of mixing under a second shear stress which is up to 1/2 of the first shear stress for at least 2 minutes. The silicone rubber base is sufficiently shelf stable to minimize a viscosity rise with time.

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## Description

This invention relates to a method for preparing a liquid silicone rubber base useful as a source of silicone rubber and a method for preparing a liquid silicone rubber composition therefrom.

In the current silicone rubber market, liquid silicone rubber compositions enjoy an increasing share since they are smoothly flowing, readily applicable through injection molding machines and amenable to automatic processing. Among others, addition curing type liquid silicone rubber compositions based on alkenyl group-containing organopolysiloxane are in widespread use. Their preparation methods are generally adapted for high manufacturing yield and flexibility for the manufacture of various types of products. Typically, a liquid silicone rubber base is first prepared as a common intermediate before a particular silicone rubber composition is prepared by blending the base with an appropriate curing agent and other ingredients.

The liquid silicone rubber base is generally prepared by blending an alkenyl-containing organopolysiloxane as a base component with a large amount of reinforcing silica filler. In JP-B 28737/1993, for example, a silicone rubber composition for injection molding is prepared by blending 100 parts by weight of organopolysiloxane with up to 300 parts by weight of a filler, typified by finely divided silica.

However, when a large amount of reinforcing silica filler is blended to form a liquid silicone rubber base from which a liquid silicone rubber composition is prepared, products having stable physical properties are not obtained unless the silica filler is previously sufficiently surface treated or the silica filler is heat treated at relatively high temperature for a long time in the presence of a surface treating agent. JP-A 238228/1995, for example, discloses the addition of hexamethyldisilazane and heat treatment at room temperature for 1 hour and then at a temperature of 100 to 250°C for at least 2 hours for restraining a viscosity increase with the lapse of time and imparting satisfactory shelf stability. Also JP-A 130344/1986 discloses heating/mixing treatment at 150°C for 2 to 3 hours. In either case, the processing time taken from the mixing of silicone oil as a base component with an inorganic filler to the completion of a base polymer is crucial. Heavy kneading or long-term heat treatment must be carried out to increase the rubber strength of the resulting liquid silicone rubber base polymer. A further long time is required in larger scale mass manufacturing plants.

Active research works have recently been made on the continuous process which generally relies on kneading operation using a continuous kneading machine such as a single or twin screw extruder. In the continuous kneading machine, a certain limit is imposed on the ratio of the shaft length to the screw diameter since kneading is carried out while applying significant shear rates by high speed rotation. The residence time in the continuous kneading machine is naturally limited, generally from several tens of seconds to several minutes. Accordingly, a sufficient processing time is not ensured. As a result, the liquid silicone rubber base undergoes a viscosity increase and loses shelf stability. A liquid silicone rubber composition prepared from the base suffers from losses of basic rubber properties such as elongation and tensile strength and losses of fatigue endurance due to insufficient dispersion of the filler.

JP-B- 28008/1992 discloses an attempt at heating a mixing section of a twin screw extrusion mixer at 200 to 300°C, thereby processing liquid silicone rubber base at a higher temperature to compensate for a shortage of processing time. Although this improves the rubber strength (tensile strength and elongation) of the resulting liquid silicone rubber composition, problems still remain with respect to viscosity and shelf stability. The liquid silicone rubber base and a liquid silicone rubber composition prepared from the base experience a change of flow with time. It is difficult to obtain a liquid silicone rubber base of stabilized quality.

The aim herein is to provide new and useful methods for preparing liquid silicone rubber base containing silica filler. Insofar as the resulting silicone rubber base materials may have new properties, these also are an aspect of the innovation. Further processings of the materials are another aspect. Particular preferred aims include, independently;

- speedy convenient preparation
- good filler dispersion
- good viscosity and shelf stability.

According to the invention, a liquid silicone rubber base is prepared by mixing organopolysiloxane containing at least two alkenyl groups attached to a silicon atom in a molecule and having a viscosity of 100 to 300,000 centistokes at 25°C, a reinforcing silica filler having a specific surface area of at least 50 m<sup>2</sup>/g as measured by the BET method, and optionally, a mixing assistant for facilitating the mixing of the organopolysiloxane with the reinforcing silica filler. We have found that when a first stage of mixing is carried out under a first shear stress of at least 1x10<sup>6</sup> N/m<sup>2</sup> and a second stage of mixing carried out under a second shear stress which is up to 1/2 of the first shear stress, we can obtain a liquid silicone rubber base which is sufficiently shelf stable to minimize a viscosity rise during shelf storage. A liquid silicone rubber composition can be prepared from the liquid silicone rubber base.

Specifically, the present invention provides a method for preparing a liquid silicone rubber base by mixing an organopolysiloxane containing at least two alkenyl groups attached to a silicon atom in a molecule and having a viscosity

of 100 to 300,000 centistokes at 25°C, reinforcing silica having a specific surface area of at least 50 m<sup>2</sup>/g as measured by the BET method, and optionally, a mixing assistant, wherein the mixing step includes a first stage of mixing under a first shear stress of at least 1x10<sup>6</sup> N/m<sup>2</sup> and a second stage of mixing under a second shear stress which is up to 1/2 of the first shear stress. Preferably heat treatment is carried out concurrent with the first and second stages of mixing. Specifically, the first stage of mixing is partially carried out at a temperature of 150 to 300°C, and the second stage of mixing is partially or entirely carried out at a temperature of 150 to 300°C. In a further preferred embodiment, the first stage of mixing continues for less than 5 minutes, the second stage of mixing continues for at least 2 minutes, and the overall mixing time of the first and second stages is at least 2.5 minutes. The first and second stages of mixing may be successively and continuously carried out through two serially connected mixers. Differently stated, the residence time in the first mixer is less than 5 minutes and the residence time in the second mixer is at least 2 minutes. We find that a silicone rubber base having good shelf stability (in that the viscosity rise after shelf storage is low) can be prepared within a relatively short time.

The present invention also provides a method for preparing a liquid silicone rubber composition by blending the liquid silicone rubber base with an organohydrogenpolysiloxane and an addition reaction catalyst. The composition exhibits good cured properties.

#### FURTHER EXPLANATION; OPTIONAL AND PREFERRED FEATURES

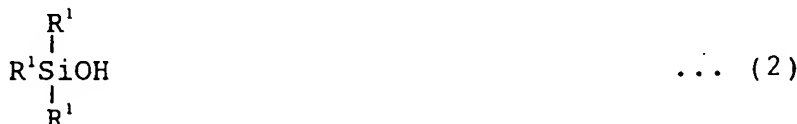
The liquid silicone rubber base and the liquid silicone rubber composition according to the invention contain an organopolysiloxane as a base component. The organopolysiloxane should contain at least two alkenyl groups attached to a silicon atom in a molecule and have a viscosity of 100 to 300,000 centistokes at 25°C. The preferred organopolysiloxane is of the following average compositional formula (1).



In formula (1), R is selected from substituted or unsubstituted monovalent hydrocarbon groups of 1 to 12 carbon atoms, especially 1 to 8 carbon atoms attached to a silicon atom, for example, alkyl groups such as methyl, ethyl, propyl, isopropyl, butyl, pentyl, and hexyl; cycloalkyl groups such as cyclopentyl, cyclohexyl, and cycloheptyl; alkenyl groups such as vinyl and allyl; aryl groups such as phenyl, tolyl, naphthyl and biphenyl; aralkyl groups such as benzyl; and substituted ones of these groups wherein some or all of the hydrogen atoms are replaced by halogen atom or cyano group. At least two R groups are alkenyl groups. Letter *a* is a positive number of 1.8 to 2.2. The structure of the organopolysiloxane is preferably linear and has an alkenyl group at an end of its molecular chain although a branched structure may be partially included. These organopolysiloxanes are of course very well known.

Silica powder having a specific surface area of at least 50 m<sup>2</sup>/g as measured by the BET method is used as a reinforcing filler. Exemplary silica fillers are fumed silica, precipitated silica and hydrophobic silica. These fillers may be used alone or in admixture of two or more. Also useful is modified silica powder obtained by incorporating silicone oil into silica powder to increase a bulk density. Silica may have been treated with surface treating agents such as hexamethyldisilazane, trimethylsilanol, dimethylsilanol, trimethylsilane, dimethylsilane, and relatively short chain siloxane having a terminal silanol group. The reinforcing silica filler is preferably blended in an amount of about 5 to 150 parts, especially about 20 to 100 parts by weight per 100 parts by weight of the organopolysiloxane.

If necessary, a mixing assistant is blended for facilitating the mixing of the organopolysiloxane with the reinforcing silica filler. This is typically a liquid substance and preferably selected from hexamethyldisilazane, compounds of the following formula (2), aqueous ammonia, and mixtures thereof.



In formula (2), R<sup>1</sup> is a monovalent hydrocarbon group as defined for R, typically methyl and vinyl, or a triorganosiloxy group such as trimethylsiloxy.

A liquid silicone rubber base is prepared by mixing the organopolysiloxane containing at least two alkenyl groups attached to a silicon atom in a molecule, the reinforcing silica filler having a BET specific surface area of at least 50 m<sup>2</sup>/g, and optionally, the mixing assistant for facilitating the mixing of the organopolysiloxane with the filler, all as defined

above.

A relatively high shear stress type mixer is used in a first stage whereby mixing is carried out under a first shear stress of at least  $1 \times 10^6$  N/m<sup>2</sup>. High shear stress mixing is effective for imparting basic rubber strength such as tensile strength and elongation to the silicone rubber. A first shear stress of less than  $1 \times 10^6$  N/m<sup>2</sup> achieves insufficient mixing and dispersion of the organopolysiloxane and silica filler, failing to ensure basic rubber strength such as tensile strength and elongation.

The first stage of mixing is mainly intended to establish rubber strength and thus requires application of relatively high shear stresses. The kneader or mixer used in the first stage of mixing may be any of mixers capable of mixing under a high shear stress of at least  $1 \times 10^6$  N/m<sup>2</sup>. In general, single, twin and multi-screw continuous extrusion kneaders are useful. Commercially available exemplary mixers are a KRC kneader by Kurimoto Iron Works K.K., a TEM twin-screw mixing extruder by Toshiba Machinery K.K., and a KCK continuous mixing extruder by KCK K.K. By means of e.g. a relatively low shear stress type mixer, serially connected to the mixer of the first stage, a second stage of mixing is successively carried out under a second shear stress which is up to  $\frac{1}{2}$  of the first shear stress, for achieving ripening of the mixture. The resulting liquid silicone rubber base has shelf stability, keeping down viscosity rise during shelf storage. The liquid silicone rubber base is ready for the preparation of a liquid silicone rubber composition therefrom. While the first stage mixer carries out mixing at a high shear stress and high shear rate and thus scarcely contributes to shelf stability, the second stage of mixing is mainly intended to insure a ripening time necessary for improving shelf stability, preferably a processing time with concomitant heating. In this regard, an unnecessarily high shear stress is undesirable for the second stage of mixing from the standpoints of energy and residence time. If a mixer capable of mixing under an equivalent shear stress to the first stage mixer were used in the second stage, the second stage mixer would be an uneconomical large one.

Thus, mixing shear stress in the second stage is not more than  $\frac{1}{2}$  that in the first stage. It may be not more than a  $\frac{1}{10}$  of that in the first stage. Usually it will be less than  $1 \times 10^6$  N/m<sup>2</sup>. Usually the residence time is greater than that in the first stage, e.g. at least twice as long. It may be 10 minutes or more.

A second stage mixer connected to a first stage mixer may be any of mixers capable of mixing under a lower shear stress. Since the second stage of mixing is intended to ensure that the liquid silicone rubber base is shelf stable so as to prevent the base from increasing its viscosity with the lapse of time, residence time is of more importance than the shear stress. Although it is fully acceptable for the second stage mixer to reduce the revolution of a rotating blade (e.g., screw and paddle) for lowering the shear rate and shear stress, the second stage mixer should preferably have a residence time of at least 2 minutes. Furthermore the mixing section of the second stage mixer should preferably be heated.

First and second stage mixers preferably carry out heat treatment concurrently with mixing for a part of the first stage of mixing and for a part or the entirety of the second stage of mixing. The heat treatment is preferably at a temperature of 150 to 300°C, more preferably 200 to 300°C. A heat treatment temperature of lower than 150°C would be less rapid in rendering hydrophobic the reinforcing silica filler containing much silanol groups which can cause a viscosity rise with time. A heat treatment temperature of higher than 300°C may deteriorate certain organopolysiloxanes as base component, for example by causing the liberation of alkenyl groups from silicon atoms in its molecule, or scission of the polymer backbone chain. Thus, temperatures in the range 150 to 300°C are usually most appropriate for ensuring shelf stability to the liquid silicone rubber base.

Desirably, an initial mixing portion of the first stage of mixing immediately after the blending of the components is maintained at a relatively low temperature, e.g. lower than 60°C.

In one preferred embodiment of the invention, the first stage of mixing continues for less than 5 minutes and the second stage of mixing continues for at least 2 minutes. The overall mixing time of the two stages is preferably at least 2.5 minutes, especially 10 to 30 minutes. Thus, in the embodiment using two serially connected extrusion mixers, preferably the residence time in the first mixer is within 5 minutes, the residence time in the second mixer is at least 2 minutes, and the total residence time is at least 2.5 minutes. Since the first stage mixer must apply a high shear stress of at least  $1 \times 10^6$  N/m<sup>2</sup>, the residence time through a continuous extrusion mixer wherein the ratio (L/D) of screw length L to screw diameter D is limited is given an upper limit. However, a certain processing time is necessary to ensure shelf stability to the liquid silicone rubber base. So, a substantial residence time can be set in the second stage mixer which carries out mixing at a relatively low shear stress and is relatively free of processing restrictions. The total residence time through the first and second stage mixers is preferably at least 2.5 minutes and more preferably at least 10 minutes, if possible. A preferred total residence time through the two mixers of at least 2.5 minutes assists production of rubber base having good shelf stability to minimize a viscosity rise with time, nevertheless within a relatively short time as compared with prior art methods. A liquid silicone rubber composition prepared from the base can also be shelf stable e.g. as compared with prior art ones.

A liquid silicone rubber composition is prepared by blending the thus obtained liquid silicone rubber base with an organohydrogenpolysiloxane and an addition reaction catalyst. The organohydrogenpolysiloxane used herein may be selected from those well known for conventional addition reaction type liquid silicone rubber compositions and added

in an effective amount for curing. The addition reaction catalyst used herein is typically a platinum series catalyst as is well known in the art. The catalyst is added in a catalytic amount. Any well-known mixing techniques may be used in blending the silicone rubber base with the organohydrogenpolysioxane and the catalyst.

In our work we find that a liquid silicone rubber base having sufficient shelf stability to minimize a viscosity rise with time can be prepared within a relatively short time as compared with prior art methods. Also a liquid silicone rubber composition which exhibits good cured properties can be prepared from the liquid silicone rubber base.

### EXAMPLE

Examples are given below to illustrate the advantages of the invention. All parts are by weight and the viscosity is a measurement at 25°C.

A liquid silicone rubber base was measured for viscosity by means of a Type B rotational viscometer by Tokyo Keiki K.K. before and after heating at 60°C for 10 days, that is, initial viscosity and viscosity at 60°C/10 days. A silicone rubber composition was prepared from the base and cured into a rubber sheet, which was measured for hardness by means of a Type A spring hardness tester according to JIS K-6301. A dumbbell No. 2 specimen was punched out of the cured rubber sheet and measured for tensile strength and elongation by means of a tensile tester by Ueshima Mfg. K.K.

#### Example 1

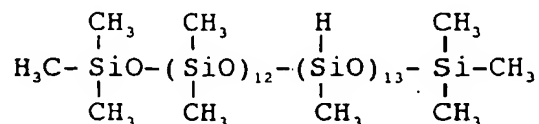
A liquid silicone rubber base was prepared by blending 60 parts of a linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as a base component, 40 parts of silica powder Nipsil LP (Nippon Silica K.K.) as a reinforcing filler, 3 parts of hexamethyldisilazane as a mixing assistant, and 1 part of water. Disposed at a first stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^7$  N/m<sup>2</sup>. The extruder had a screw diameter D of 50 mm and a L/D ratio of 50/1. The extruder defined a mixing section of a length extending from the inlet to the outlet. An upstream portion extending from the inlet to 30% of the length was set at a temperature below 50°C, a succeeding 5% portion at 100°C, a further succeeding 5% portion at 200°C, and the remainder extending to the outlet at 250°C.

Serially disposed at a second stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^5$  N/m<sup>2</sup>. The extruder had a screw diameter D of 150 mm and a L/D ratio of 10/1. The extruder was kept at 250°C equal to the downstream portion of the first stage extruder.

The residence time was 1.5 minutes through the first stage extruder and 20 minutes through the second stage extruder. The total residence time was 21.5 minutes.

The liquid silicone rubber base, 110 parts, was diluted with 25 parts of the linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as the base component, and cooled.

A liquid silicone rubber composition was prepared by blending the liquid silicone rubber base with 4 parts of methylhydrogenpolysiloxane of the formula:



0.3 part of a 2% 2-ethylhexanol solution of chloroplatinic acid, and 0.2 part of ethynyl cyclohexanol as a reaction inhibitor. The composition was cured at 120°C for 10 minutes into a sheet of 2 mm thick.

Table 1 shows the viscosity behavior of the liquid silicone rubber base and the physical properties of the cured sheet.

#### Example 2

A liquid silicone rubber base was prepared by blending 60 parts of a linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as a base component, 40 parts of silica powder Nipsil LP (Nippon Silica K.K.) as a reinforcing filler, 3 parts of hexamethyldisilazane as a mixing assistant, and 1 part of water. Disposed at a first stage was a twin screw continuous mixing extruder in which

the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^7$  N/m<sup>2</sup>. The extruder had a screw diameter D of 50 mm and a L/D ratio of 50/1. An upstream portion of the extruder extending from the inlet to 30% of the length was set at a temperature below 50°C, a succeeding 5% portion at 100°C, a further succeeding 5% portion at 200°C, and the remainder extending to the outlet at 250°C.

Serially disposed at a second stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^4$  N/m<sup>2</sup>. The extruder had a screw diameter D of 150 mm and a L/D ratio of 10/1. The extruder was kept at 250°C equal to the downstream portion of the first stage extruder.

The residence time was 1.5 minutes through the first stage extruder and 6 minutes through the second stage extruder. The total residence time was 7.5 minutes.

The liquid silicone rubber base, 110 parts, was diluted with 25 parts of the linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as the base component, and cooled.

A liquid silicone rubber composition was similarly prepared from the liquid silicone rubber base.

The viscosity behavior and physical properties were measured as in Example 1, with the results shown in Table 1.

### Example 3 (Comparative)

A liquid silicone rubber base was prepared by blending 60 parts of a linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as a base component, 40 parts of silica powder Nipsil LP (Nippon Silica K.K.) as a reinforcing filler, 3 parts of hexamethyldisilazane as a mixing assistant, and 1 part of water. Disposed at a first stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^4$  N/m<sup>2</sup>. The extruder had a screw diameter D of 50 mm and a L/D ratio of 50/1. An upstream portion of the extruder extending from the inlet to 30% of the length was set at a temperature below 50°C, a succeeding 5% portion at 100°C, a further succeeding 5% portion at 200°C, and the remainder extending to the outlet at 250°C.

Serially disposed at a second stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^4$  N/m<sup>2</sup>. The extruder had a screw diameter D of 150 mm and a L/D ratio of 10/1. The extruder was kept at 250°C equal to the downstream portion of the first stage extruder.

The residence time was 1.5 minutes through the first stage extruder and 20 minutes through the second stage extruder. The total residence time was 21.5 minutes.

The liquid silicone rubber base, 110 parts, was diluted with 25 parts of the linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as the base component, and cooled.

A liquid silicone rubber composition was similarly prepared from the liquid silicone rubber base.

The viscosity behavior and physical properties were measured as in Example 1, with the results shown in Table 1.

### Example 4

A liquid silicone rubber base was prepared by blending 60 parts of a linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as a base component, 40 parts of silica powder Nipsil LP (Nippon Silica K.K.) as a reinforcing filler, 3 parts of hexamethyldisilazane as a mixing assistant, and 1 part of water. Disposed at a first stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^7$  N/m<sup>2</sup>. The extruder had a screw diameter D of 50 mm and a L/D ratio of 50/1. An upstream portion of the extruder extending from the inlet to 30% of the length was set at a temperature below 50°C, a succeeding 5% portion at 100°C, a further succeeding 5% portion at 200°C, and the remainder extending to the outlet at 250°C.

Serially disposed at a second stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^5$  N/m<sup>2</sup>. The extruder had a screw diameter D of 150 mm and a L/D ratio of 10/1. The extruder was kept at 120°C.

The residence time was 1.5 minutes through the first stage extruder and 20 minutes through the second stage extruder. The total residence time was 21.5 minutes.

The liquid silicone rubber base, 110 parts, was diluted with 25 parts of the linear dimethylpolysiloxane blocked with

a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as the base component, and cooled.

A liquid silicone rubber composition was similarly prepared from the liquid silicone rubber base.

The viscosity behavior and physical properties were measured as in Example 1, with the results shown in Table 1.

#### Example 5

A liquid silicone rubber base was prepared by blending 60 parts of a linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as a base component, 40 parts of silica powder Nipsil LP (Nippon Silica K.K.) as a reinforcing filler, 3 parts of hexamethyldisilazane as a mixing assistant, and 1 part of water. Disposed at a first stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^7$  N/m<sup>2</sup>. The extruder had a screw diameter D of 50 mm and a L/D ratio of 50/1. An upstream portion of the extruder extending from the inlet to 30% of the length was set at a temperature below 50°C, a succeeding 5% portion at 100°C, a further succeeding 5% portion at 200°C, and the remainder extending to the outlet at 250°C.

Serially disposed at a second stage was a twin screw continuous mixing extruder in which the revolution of screws and paddles and the clearance between the screws and paddles and the barrel were adjusted to apply a shear stress of about  $1 \times 10^5$  N/m<sup>2</sup>. The extruder had a screw diameter D of 150 mm and a L/D ratio of 10/1. The extruder was kept at 250°C equal to the downstream portion of the first stage extruder.

The residence time was 1.2 minutes through the first stage extruder and 1.2 minutes through the second stage extruder. The total residence time was 2.4 minutes.

The liquid silicone rubber base, 110 parts, was diluted with 25 parts of the linear dimethylpolysiloxane blocked with a methylvinylsilyl group at each end of its molecular chain having a viscosity of 10,000 centistokes as the base component, and cooled.

A liquid silicone rubber composition was similarly prepared from the liquid silicone rubber base.

The viscosity behavior and physical properties were measured as in Example 1, with the results shown in Table 1.

Table 1

Example	Viscosity (poise) of liquid silicone rubber base		Hardness (JIS A)	Tensile strength (kgf/cm <sup>2</sup> )	Elongation (%)
	Initial	60°C/10 days			
1	650	650	40	78	350
2	700	790	40	75	310
3	850	980	42	35	190
4	800	3000	43	68	300
5	750	3200	43	60	280

#### Claims

1. A method for preparing a liquid silicone rubber base comprising a step of mixing organopolysiloxane, having at least two silicon-bonded alkenyl groups per molecule and viscosity in the range 100 to 300,000 centistokes at 25°C, with reinforcing silica having a specific surface of at least 50 m<sup>2</sup>/g BET,

characterized in that the step of mixing includes a first stage of mixing at shear stress of at least  $1 \times 10^6$  N/m<sup>2</sup> followed by a second stage of mixing at shear stress not more than half that in the first stage.

2. A method according to claim 1 including applying heat as the mixing proceeds.

3. A method according to claim 2 in which the first stage of mixing occurs at least partially at a temperature in the range 150°C to 300°C.

4. A method according to claim 2 or claim 3 in which the second stage of mixing occurs at least partially at a temperature in the range 150°C to 300°C.

5. A method according to any one of the preceding claims in which the first stage of mixing lasts for less than 5 minutes.
6. A method according to any one of the preceding claims in which the second stage of mixing lasts for at least 2 minutes.
7. A method according to any one of the preceding claims in which the overall mixing time of the first and second stage is at least 2.5 minutes.
8. A method according to claim 7 in which said overall mixing time is at least 10 minutes.
9. A method according to any one of the preceding claims in which the step of mixing is carried out on a continuous basis, with the first and second stages of mixing being carried out respectively in first and second extrusion mixers connected in series.
10. A method according to any one of the preceding claims in which a mixing assistant is blended for the step of mixing.
11. A method of making a curable liquid silicone rubber composition comprising blending a silicone rubber base obtained in accordance with any one of claims 1 to 10 with an organohydrogenpolysiloxane and an addition reaction catalyst.
12. A method according to claim 11 further comprising curing the rubber composition to form a cured, shaped silicone rubber article.



(19)



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(54) **Methods for the preparation of liquid silicone rubber base and liquid silicone rubber composition**

(57) A liquid silicone rubber base is prepared by mixing an organopolysiloxane containing at least two alkenyl groups, reinforcing silica having a BET specific surface area of at least 50 m<sup>2</sup>/g, and optionally, a mixing assistant. The mixing step includes a first stage of mix-

ing under a first shear stress of at least 1x10<sup>6</sup> N/m<sup>2</sup> for 1-5 minutes and a second stage of mixing under a second shear stress which is up to 1/2 of the first shear stress for at least 2 minutes. The silicone rubber base is sufficiently shelf stable to minimize a viscosity rise with time.

**EP 0 846 720 A3**



European Patent  
Office

## EUROPEAN SEARCH REPORT

Application Number  
EP 97 30 9836

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.6)
A	EP 0 691 373 A (DOW CORNING) 10 January 1996 * example 1 *	1	C08K3/36 C08K9/06 C08L83/07
A	EP 0 462 032 A (RHONE-POULENC) 18 December 1991 * claim 1 *	1	
A	GB 2 284 609 A (GENERAL ELECTRIC) 14 June 1995 * claim 1 *	1	
			TECHNICAL FIELDS SEARCHED (Int.Cl.6)
			C08K C08L
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 26 June 1998	Examiner Lentz, J
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document			

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